

- 1) Blasius solution to the laminar boundary layer equations yields

$$v = \frac{1}{2} \sqrt{\frac{\nu U_\infty}{x}} (\eta f' - f)$$

For the vertical velocity where the stream function  $\psi = f(\eta) \sqrt{\nu x U_\infty}$  and  $\eta = y \sqrt{\frac{U_\infty}{\nu x}}$

- Verify the expression for  $v$
- Find the  $x$  component of the acceleration  $a_x$  in terms of  $f$ ,  $x$  and  $U_\infty$
- Find the expression for the wall shear stress in terms of  $f$  and  $\eta$
- Find an algebraic expression for the total viscous drag for a flat plate of length  $L$  and width  $w$

**Solution:**

a)

$$\frac{\partial \eta}{\partial x} = -\frac{y}{2} \sqrt{\frac{U_\infty}{x^3 \nu}}, \frac{\partial \eta}{\partial y} = \sqrt{\frac{U_\infty}{\nu x}}, u = \frac{\partial \psi}{\partial y} = f'(\eta) \frac{\partial \eta}{\partial y} \sqrt{\nu x U_\infty} = f'(\eta) \sqrt{\frac{U_\infty}{\nu x}} \sqrt{\nu x U_\infty} = U_\infty f'(\eta)$$

$$\begin{aligned} v &= -\frac{\partial \psi}{\partial x} = -\left( f'(\eta) \frac{\partial \eta}{\partial x} \sqrt{\nu x U_\infty} + \frac{f(\eta)}{2} \sqrt{\frac{\nu U_\infty}{x}} \right) = -\left( f'(\eta) \left( -\frac{y}{2} \sqrt{\frac{U_\infty}{x^3 \nu}} \right) \sqrt{\nu x U_\infty} + \frac{f(\eta)}{2} \sqrt{\frac{\nu U_\infty}{x}} \right) \\ &= \frac{1}{2} \sqrt{\frac{\nu U_\infty}{x}} \left( f'(\eta) \left( y \sqrt{\frac{U_\infty}{\nu x}} \right) - f(\eta) \right) = \frac{1}{2} \sqrt{\frac{\nu U_\infty}{x}} (\eta f' - f) \end{aligned}$$

b)

$$\begin{aligned} a_x &= \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = 0 + U_\infty f'(\eta) U_\infty f''(\eta) \frac{\partial \eta}{\partial x} + \frac{1}{2} \sqrt{\frac{\nu U_\infty}{x}} (\eta f' - f) U_\infty f''(\eta) \frac{\partial \eta}{\partial y} \\ &= U_\infty f'(\eta) U_\infty f''(\eta) \left( -\frac{y}{2} \sqrt{\frac{U_\infty}{x^3 \nu}} \right) + \frac{1}{2} \sqrt{\frac{\nu U_\infty}{x}} (\eta f' - f) U_\infty f''(\eta) \sqrt{\frac{U_\infty}{\nu x}} \\ &= \frac{U_\infty^2 f''(\eta)}{2x} \left( f'(\eta) \left( -y \sqrt{\frac{U_\infty}{\nu x}} \right) + (\eta f' - f) \right) = -\frac{U_\infty^2 f f''}{2x} \end{aligned}$$

c)

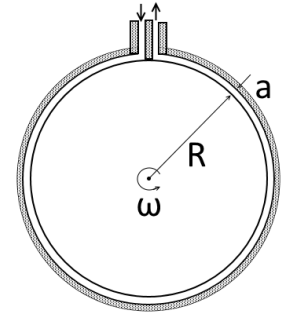
$$\tau = \mu \frac{\partial u}{\partial y} = \mu U_\infty f''(\eta) \frac{\partial \eta}{\partial y} = \mu U_\infty f''(\eta) \sqrt{\frac{U_\infty}{\nu x}}, \quad \tau_w = \frac{\mu U_\infty^{\frac{3}{2}} f''(0)}{\sqrt{\nu x}}$$

d) Drag on one side

$$F = w \int_0^L \tau_w dx = w \frac{\mu U_\infty^{\frac{3}{2}} f''(0)}{\sqrt{\nu}} \int_0^L \frac{dx}{\sqrt{x}} = w \frac{\mu U_\infty^{\frac{3}{2}} f''(0)}{\sqrt{\nu}} 2\sqrt{L} = 2f''(0) w U_\infty^{\frac{3}{2}} \sqrt{\rho \mu L} = \frac{2f''(0)}{\sqrt{Re}} \rho U_\infty^2 w L$$

- 2) Consider a viscous shear pump made from a stationary housing with a close-fitting rotating drum inside. The clearance  $a$  is small compared to the radius  $R$  so that flow in the annular space may be treated as flow between parallel plates.

- a) Find the pressure differential  $\Delta p$   
 b) Input power  $P_{in}$   
 c) Power output  $P_{out}$  and efficiency  $P_{out}/P_{in}$   
 As functions of volumetric flow rate per unit length  
 ( $Q/b$  where  $b$  is the length of the drum)



**Solution:**

a)

$$\frac{\partial p}{\partial x} = \mu \frac{\partial^2 u}{\partial y^2} \rightarrow \frac{\partial u}{\partial y} = \frac{1}{\mu} \frac{\partial p}{\partial x} y + c_1 \rightarrow u = \frac{1}{2\mu} \frac{\partial p}{\partial x} y^2 + c_1 y + c_2$$

$$y = 0, u = 0 \rightarrow c_2 = 0, \quad y = a, u = \omega R \rightarrow \omega R = \frac{1}{2\mu} \frac{\partial p}{\partial x} a^2 + c_1 a \rightarrow c_1 = \frac{\omega R}{a} - \frac{1}{2\mu} \frac{\partial p}{\partial x} a$$

$$u = \frac{1}{2\mu} \frac{\partial p}{\partial x} y^2 + \left( \frac{\omega R}{a} - \frac{1}{2\mu} \frac{\partial p}{\partial x} a \right) y = \frac{1}{2\mu} \frac{\partial p}{\partial x} (y^2 - ay) + \frac{\omega R}{a} y$$

$$\frac{Q}{b} = \int_0^a u dy = \left( \frac{1}{2\mu} \frac{\partial p}{\partial x} \left( \frac{y^3}{3} - a \frac{y^2}{2} \right) + \frac{\omega R y^2}{2} \right) \Big|_0^a = \frac{1}{2\mu} \frac{\partial p}{\partial x} \left( -\frac{a^3}{6} \right) + \frac{\omega R a^2}{2}$$

$$\frac{1}{2\mu} \frac{\partial p}{\partial x} \left( -\frac{a^3}{6} \right) = \frac{Q}{b} - \frac{a\omega R}{2}, \quad -\frac{\partial p}{\partial x} = -\frac{\Delta p}{2\pi R} = \frac{12\mu}{a^3} \left( \frac{Q}{b} - \frac{a\omega R}{2} \right)$$

$$\Delta p = \frac{24\pi R\mu}{a^3} \left( \frac{a\omega R}{2} - \frac{Q}{b} \right) = \frac{12\pi R^2\mu\omega}{a^2} \left( 1 - \frac{2Q}{a\omega Rb} \right)$$

b) Per unit length power

$$P_{in} = \frac{T\omega}{b} = \tau_w LR\omega = \mu \frac{\partial u}{\partial y} \Big|_{y=a} LR\omega = \mu \left( \frac{\omega R}{a} + \frac{1}{2\mu} \frac{\Delta p}{2\pi R} a \right) 2\pi R^2 \omega$$

$$P_{in} = \mu \left( \frac{2\pi\omega R^2}{a} + \frac{a\Delta p}{2\mu} \right) R\omega = \mu \left( \frac{2\pi\omega R^2}{a} + \frac{6\pi R^2\omega}{a} \left( 1 - \frac{2Q}{a\omega Rb} \right) \right) R\omega$$

c)

$$P_{out} = \Delta p \frac{Q}{b} = \frac{12\pi R^2\mu\omega}{a^2} \left( 1 - \frac{2Q}{a\omega Rb} \right) \frac{Q}{b}$$

$$\eta = \frac{P_{out}}{P_{in}} = \frac{\frac{6}{a} \left( 1 - \frac{2Q}{a\omega Rb} \right) \frac{Q}{b}}{\left( 1 + 3 \left( 1 - \frac{2Q}{a\omega Rb} \right) \right) R\omega} = \frac{\left( 1 - \frac{2Q}{a\omega Rb} \right) 6Q}{\left( 4 - \frac{6Q}{a\omega Rb} \right) a\omega Rb}$$

$$\eta_{max} = \frac{1}{3} \text{ at } \frac{Q}{a\omega Rb} = \frac{1}{3}$$

- 3) A spherical particle, under the influence of gravity, falls very slowly through a viscous fluid.
- Find the terminal velocity of the particle in terms of  $\rho_{\text{particle}}$ ,  $\rho_{\text{fluid}}$ ,  $D$  and  $\mu$ .
  - Calculate the velocity for the given values below and check the validity of your assumptions

$$\rho_{\text{particle}} = 4000 \frac{\text{kg}}{\text{m}^3}, \quad \rho_{\text{fluid}} = 800 \frac{\text{kg}}{\text{m}^3}, \quad D = 0.5 \text{ mm}, \quad \mu = 0.1 \frac{\text{kg}}{\text{m}\cdot\text{s}}$$

**Solution:**

$$W = (\rho_p - \rho_f)gVol = (\rho_p - \rho_f)g \frac{4}{3}\pi\left(\frac{D}{2}\right)^3$$

$$D = C_D \frac{1}{2} \rho_f V^2 A = \frac{24}{Re} \frac{1}{2} \rho_f V^2 \pi \left(\frac{D}{2}\right)^2 = 3\pi\mu VD$$

$$W = D \rightarrow V = \frac{g}{18\mu} (\rho_p - \rho_f) D^2 = 0.00436 \frac{\text{m}}{\text{s}}$$

$$Re = \frac{\rho_f VD}{\mu} = 0.0174 \ll 1$$